Simulation of Synthetic Jets Using Unsteady Reynolds-Averaged Navier–Stokes Equations

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An unsteady Reynolds-averaged Navier–Stokes solver is applied for the simulation of a synthetic (zero net mass flow) jet created by a single diaphragm piezoelectric actuator in quiescent air. This configuration was designated as case 1 for the Computational Fluid Dynamics Validation 2004 (CFDVAL2004) workshop held at Williamsburg, Virginia, in March 2004. Time-averaged and instantaneous (phase-averaged) data for this case were obtained at NASA Langley Research Center, using multiple measurement techniques. Computational results from two-dimensional simulations with one-equation Spalart–Allmaras and two-equation Menter's turbulence models are presented along with the experimental data. The effect of grid refinement, preconditioning, and time-step variation are also examined.

Introduction

SIGNIFICANT interest has been growing in the aerospace community in the field of flow control in recent years. An entire AIAA conference is now devoted every other year to this field. In March 2004, NASA Langley Research Center, in conjunction with five other international organizations, held the Computational Fluid Dynamics Validation 2004 (CFDVAL2004) workshop[1] in Williamsburg, Virginia. The primary objective of this workshop was to assess the state of the art for measuring and computing aerodynamic flows in the presence of synthetic jets. Thomas et al.[2] have conducted an exhaustive and comprehensive survey identifying the feasibility of using active flow control to improve the performance of both external and internal flows. Suggested applications cover a wide range from smart materials and microelectromechanical systems to synthetic (zero net mass flow) jets for enhancing control forces, reducing drag, increasing lift, and enhancing mixing. It is also conjectured that active flow control would permit the use of thicker wing sections in nonconventional configurations, such as the blended wing body configuration, without compromising the aerodynamic performance.

Most of the research in the area of active flow control is of an empirical nature, partially due to the cost and lack of confidence in computational methods for such complex flows. However, without the availability of efficient and well-calibrated computational tools, it will be a very difficult, expensive, and slow process to determine the optimum layout and placement for active flow control devices in practical applications. With the continuous reduction of computer costs in recent years, researchers are devoting more attention to the simulation of such unsteady flows and flow control devices from a computational fluid dynamics (CFD) point of view.[3−8] With few exceptions, most of the numerical studies are undertaken without an active interaction with experimental investigators. Comparisons with experimental data are sometimes done years after the experimental data have been acquired. Under such a scenario, one has to reconstruct many of the details about the experimental arrangement and boundary conditions without the benefit of concrete and consistent information. Based on our experience from previous validation exercises,[9] we recognized the need for active collaboration of the computational and experimental research. Without a symbiotic relationship between the two groups, major misunderstandings can develop when results from these disciplines differ significantly. We were very fortunate to have a cooperative relationship with the researchers conducting the experiments, as well as access to pertinent experimental data.

Our primary objective for this work is to calibrate an existing computational scheme with experimental data for the time-dependent flows encountered in active flow control environments. We devote special attention to establishing appropriate boundary conditions for such flows, especially in the absence of the detailed experimental data required for closure.

The configuration chosen for CFD validation is identified as case 1 in the CFDVAL2004 workshop[1] and represents an isolated synthetic jet formed by a single diaphragm, piezoelectric actuator exhausting into ambient quiescent air. Multiple measurement techniques, including particle image velocimetry (PIV), laser doppler velocimetry (LDV), and hot-wire probes were used to generate a large body of experimental data for this configuration. In Refs. 1 and 10 the details are described of the experimental setup and geometric configuration. In this paper, we assess the effects of grid refinement, time-step variation, preconditioning, and turbulence models on the computational simulations of the flowfield generated by this flow control device. We model the actuator cavity with a simpler configuration in the present simulations. We demonstrate and calibrate our computational method for simulating synthetic jets by comparing the numerical results with the experimental data.

Governing Equations

A generalized form of the thin-layer Navier–Stokes (N–S) equations is used to model the flow. The equation set is obtained from the complete N–S equations by neglecting the cross-derivative terms from the viscous diffusion. Such cross-diffusion terms are significant only in the very small, $\mathcal{O}(\delta \times \delta)$, corner layers and should have negligible effect on the overall accuracy. For a body-fitted coordinate system (ξ, η, ζ) fixed in time, these equations can be written in the conservative form as

$$\text{Vol}\frac{\partial(\boldsymbol{U})}{\partial t} + \frac{\partial(\boldsymbol{F} - \boldsymbol{F}_v)}{\partial \xi} + \frac{\partial(\boldsymbol{G} - \boldsymbol{G}_v)}{\partial \eta} + \frac{\partial(\boldsymbol{H} - \boldsymbol{H}_v)}{\partial \zeta} = 0 \quad (1)$$

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where U represents the conserved variable vector. The vectors F, G, and H, and F_v, G_v, and H_v are the convective and diffusive fluxes in the three transformed coordinate directions, respectively. In Eq. (1), Vol is the cell volume or the Jacobian of the coordinate transformation. A multigrid-based, multiblock, structured grid, thin-layer N–S three-dimensional flow solver TLNS3D, developed at NASA Langley Research Center is used for the solution of the governing equations. For two-dimensional configurations, the fluxes in the third coordinate, ζ, are dropped from the governing equations. In Refs. 11–13 the TLNS3D solver is described in detail; therefore, only a brief summary of its general features is included here.

Discretization

The spatial terms in Eq. (1) are discretized using a cell-centered finite volume scheme. The convection terms are discretized using second-order central differences with a matrix artificial dissipation (second- and fourth-difference dissipation) added to suppress the odd–even decoupling and oscillations in the vicinity of shock waves and stagnation points.[14−16] The viscous terms are discretized with second-order accurate central difference formulas.[11] The zero-equation model of Baldwin–Lomax,[17] one-equation model of Spalart–Allmaras,[18] and Menter's two-equation, shear stress transport (SST) model[19] are available in TLNS3D code for simulating turbulent flows. For the present computations, the Spalart–Allmaras (S–A) model and the Menter's (SST) model are used.

Regrouping the terms on the right-hand side into convective and diffusive terms, Eq. (1) can be rewritten as

$$\frac{dU}{dt} = -C(U) + D_p(U) + D_a(U) \qquad (2)$$

where $C(U)$, $D_p(U)$, and $D_a(U)$ are the convection, physical diffusion, and artificial diffusion terms, respectively. These terms include the cell volume or the Jacobian of the coordinate transformation.

The time-derivative term can be approximated to any desired order of accuracy by a Taylor series:

$$\frac{dU}{dt} = \frac{1}{\Delta t}\left[a_0 U^{n+1} + a_1 U^n + a_2 U^{n-1} + a_3 U^{n-2} + \cdots\right] \qquad (3)$$

The superscript n represents the last time level at which the solution is known, and $n + 1$ refers to the next time level to which the solution will be advanced. Similarly, $n - 1$ refers to the solution at one time level before the current solution. Equation (3) represents a generalized backward difference scheme (BDF) in time, where the order of accuracy is determined by the choice of coefficients a_0, a_1, $a_2, \ldots$, etc. For example, $a_0 = 1.5$, $a_1 = -2$, and $a_2 = 0.5$ results in a second-order accurate scheme (BDF2) in time, which is the primary scheme chosen for this work because of its unconditional stability and good robustness properties.[20] Regrouping the time-dependent terms and the original steady-state operator leads to the equation

$$\frac{a_0}{\Delta t} U^{n+1} + \frac{E(U^n, U^{n-1}, \ldots)}{\Delta t} = S(U^n) \qquad (4)$$

where $E(U^n, U^{n-1}, \ldots)$ depends only on the solution vector at time levels n and earlier. S represents the steady-state operator or the right-hand side of Eq. (2). By adding a pseudotime term, we rewrite Eq. (4) as

$$\frac{\partial U}{\partial \tau} + \frac{a_0}{\Delta t} U^{n+1} + \frac{E(U^n, U^{n-1}, \ldots)}{\Delta t} = S(U^n) \qquad (5)$$

Solution Algorithm

The algorithm for solving unsteady flow makes extensive use of the steady-state algorithm in the TLNS3D code.[11−13] The basic algorithm consists of a five-stage Runge–Kutta time stepping scheme for advancing the solution in pseudotime. Efficiency of this algorithm is enhanced through the use of local timestepping, residual smoothing, and multigrid techniques developed for solving steady-state equations. Because the Mach number in much of the domain

is very low, we consider the use of preconditioning methods[21,22] to improve the efficiency and accuracy of the flow solver.

To solve the time-dependent N–S equations, we add another iteration loop in physical time outside the pseudotime iteration loop of the steady-state solver. For fixed values of $E(U^n, U^{n-1}, \ldots)$, we iterate on U^{n+1} using the standard multigrid procedure of TLNS3D developed for steady state, until the pseudoresidual $(a_0/\Delta t)U + E(U)/\Delta t - S(U)$ approaches zero. This strategy, originally proposed by Jameson[23] for Euler equations and adapted for the TLNS3D viscous flow solver by Melson et al.,[20] is popularly known as the dual time-stepping scheme for solving unsteady flows. The process is repeated until the desired number of physical time steps is completed. The details of the TLNS3D flow code for solving unsteady flows are available in Refs. 20 and 24–26.

Boundary Conditions

For the viscous walls, we use the no-slip, no injection, zero pressure gradient and fixed-wall temperature conditions for solving the governing equations. For the inviscid walls, we specify zero normal velocity and zero pressure gradient normal to the wall. We apply Riemann invariants-based boundary conditions (see Ref. 27) at the far-field boundaries.

We apply a periodic velocity transpiration condition to simulate the effect of a moving diaphragm. The frequency of the transpiration velocity in the numerical simulation corresponds to the frequency of the oscillating diaphragm. We determined the peak transpiration velocity from numerical iteration to match the experimentally measured peak velocity at the jet exit. A zero pressure gradient is imposed at this boundary for closure. We also tested the pressure gradient boundary condition obtained from a one-dimensional normal momentum equation,[28] which had very little impact on the solutions. Because of its simplicity and robustness, we selected the zero pressure gradient boundary condition at the transpiration surface for the present computations.

We set the turbulent eddy-viscosity level equal to 1% of the molecular viscosity at the far-field and inflow boundaries. At the solid walls, the eddy viscosity is set equal to zero. Complete details on the boundary condition treatment of turbulence quantities are available in the original papers on these models.[18,19]

Synthetic Jet Test Case: Background

The test configuration examined in this paper is a single diaphragm piezoelectric actuator operating in quiescent air. The oscillatory motion of the diaphragm produces a synthetic jet that exhausts into the surrounding quiescent air. This configuration, shown in Fig. 1a, consists of a 1.27-mm-wide rectangular slot connected to a cavity with a circular piezoelectric diaphragm and corresponds to case 1 of the CFDVAL2004 workshop on flow control devices.[1] The actuator is connected to an enclosure box, such that the slot exit is perfectly matched to a rectangular hole in the base of the enclosure box. The sides of this enclosure box are 600 mm long (Fig. 2a). Although the cavity and diaphragm geometry of this actuator are highly three dimensional in the interior, the actual slot through which the fluid emerges is a high aspect ratio rectangular slot and is modeled as a two-dimensional configuration.

A two-dimensional sectional cut at the midspan location of the physical model showing the oscillating diaphragm and slot geometry is shown in Fig. 1b. A multiblock structured grid modeling this simplified geometry was used by the present authors and several of the CFDVAL2004 workshop participants for numerical simulations.[1] The diaphragm motion was simulated via a transpiration condition imposed at the diaphragm surface located at the side of the cavity. Some of the workshop participants further simplified the cavity modeling by imposing a transpiration condition at the bottom part of the slot's neck or even directly at the slot exit. After examining these results, we concluded that as long as the unsteady velocity signal at the slot exit replicates experimental conditions, details of the cavity modeling have an insignificant effect on the development of the synthetic jet emanating from the slot.[1,29]
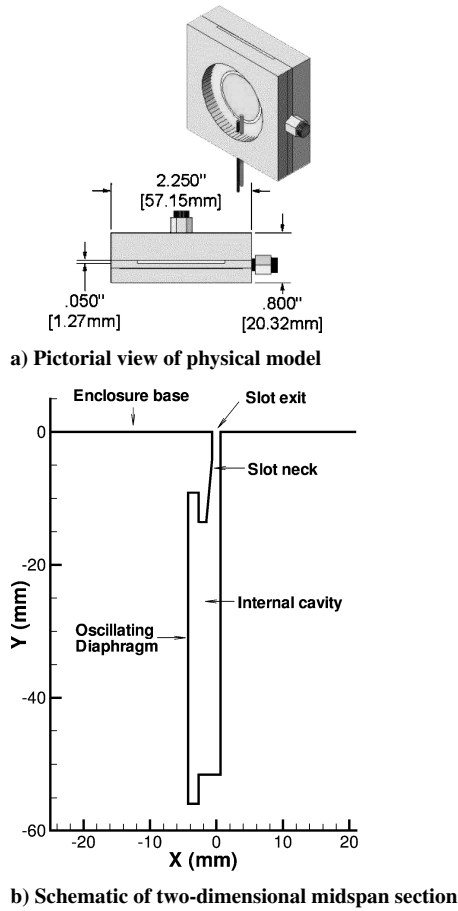
a) Pictorial view of physical model

b) Schematic of two-dimensional midspan section

Fig. 1 Schematic of piezoelectric actuator.

a) Global view

b) Detailed view

Fig. 2 Computational model of piezoelectric actuator.

Results and Discussion

One of the major difficulties identified during the CFDVAL2004 workshop was the large disparity in experimental data obtained from different measurement techniques.[1] Such a variation in experimental data made it difficult to validate the numerical methods. Part of the difficulty in acquiring a consistent set of experimental data arose from the fact that the performance of the piezoelectric diaphragm depends on ambient conditions. Also, its performance degrades over time, which means that, for a given input voltage, the actuator produces smaller jet velocities as it ages. Because these experiments were conducted over several months, inconsistencies crept into the data. Yao et al.[10] have recently revisited the synthetic jet test case and acquired experimental data for this configuration with a new piezoelectric diaphragm. They obtained the detailed field data with the PIV technique and pointwise data along the jet centerline with hot-wire and LDV techniques. They monitored the performance of the actuator regularly and demonstrated good consistency among the PIV and LDV measurement techniques.[10] However, the hot-wire measurements deviated significantly from the PIV and LDV data, especially near solid walls. For this reason, we decided to make use of only the PIV and LDV data for comparison with the computational results.

Based on the CFDVAL2004 workshop[1] results, it can be concluded that replicating the flow conditions at the slot exit is more important than the detailed modeling of cavity geometry for accurate simulation of the growth of a synthetic jet for this configuration. Therefore, we simulated the new experimental test case with a simplified cavity geometry, shown schematically in Figs. 2a and 2b. We imposed the transpiration condition at the bottom of the slot's neck to simulate the velocity generated by the oscillating diaphragm. A top-hat velocity profile, with a dominant frequency of 450 Hz replicating the experimental conditions, was imposed at this boundary. The precise temporal variation of the velocity signal was obtained by curve fitting the measured velocities at the slot exit,
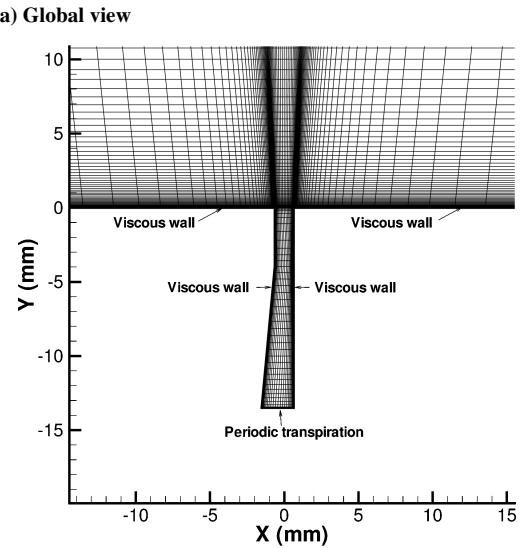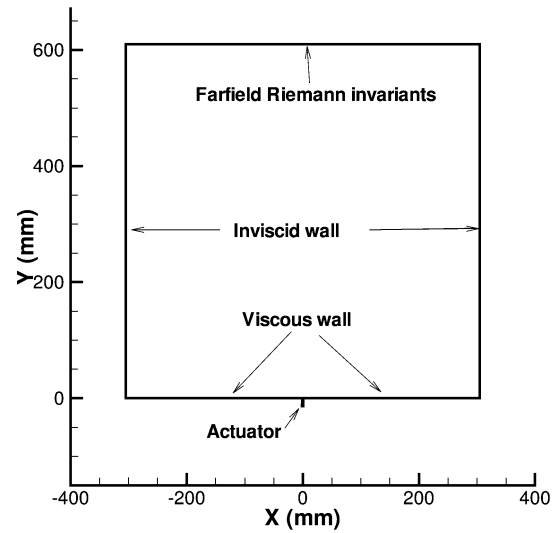
$x = 0$ and $y = 0.3$ mm, with a fast Fourier transform to reflect the proper mode shape and to ensure zero net mass transfer. The amplitude of this transpiration velocity was determined numerically to match the peak velocity at the slot exit from the experimental study of Yao et al.[10] The freestream Mach number in the exterior quiescent region is specified as $M_\infty = 0.001$ to simulate incompressible flow in the compressible flow code to avoid numerical difficulties at Mach zero. Based on the peak jet velocity and slot width, the Reynolds number is approximately 3000, a regime where the jet is expected to be turbulent. Therefore, we assumed the flow to be fully turbulent in the present computations.

A multiblock structured grid consisting of approximately 61,000 nodes is used as a baseline grid for these computations. This grid is nearly identical to the baseline grid (except for internal cavity region) used by the CFDVAL2004 workshop participants.[1] In addition, a coarse grid (CG) was created by eliminating every other point in both directions from the baseline grid. Similarly, a finer grid (FG), consisting of approximately 250,000 nodes, was created by doubling the baseline grid in both directions. To reduce computational costs, the FG solutions were run on half of the domain by imposing symmetry conditions along $x = 0$ plane, and the results were mirrored for plotting purposes about the symmetry plane. Most of the computations were performed with the one-equation SA turbulence model using 72 time steps/period corresponding to a 5-deg phase angle between the time steps. The effect of temporal resolution was assessed by performing computations with half of the baseline

time step, which required 144 time steps/period. In addition, the solutions on the baseline grid were also obtained with Menter's (SST) turbulence model. Finally, one set of computations was performed with low-speed preconditioning to assess the accuracy of the compressible flow code for computing the low-speed flows encountered in this problem.

The TLNS3D code for each case was run long enough to achieve a repeatable periodic state for the flow solutions. Starting from the converged solutions, the computations were run for 15 more complete time periods to extract long time-averaged quantities. Taking advantage of the periodic nature of flow, solutions from the last complete time period were used for phase-averaged quantities. Finally, the origin of the phase for experimental and computational results was fixed by shifting the phase angle of the vertical velocity (V-VEL) profiles near the slot exit, $x = 0$ and $y = 0.3$ mm, such that the maximum suction for the experimental and computational velocities occur at the phase of 255 deg. This procedure was applied to set the phase for all of the results presented here. Unless mentioned otherwise, the computations were performed on the baseline grid with the SA turbulence model using 72 time steps/period.

The time history of the phase-averaged V-VEL for a complete period from the computational results is compared with the experimental data in Fig. 3 at $x = 0$ and $y = 0.3$ mm. This is the closest point to the slot exit where the PIV data are available. The LDV measurements are also available at this location and are shown in Fig. 3. The overall agreement between the computational and experimental results is quite good at this location. The four sets of computational results shown in Fig. 3 are mostly indistinguishable from one another, indicating a minimal effect of grid density and turbulence model at the slot exit boundary.

In Fig. 4a, we present the computational results for time-averaged V-VEL along the jet centerline obtained with the SA turbulence model for three different grids. In addition, we present the results obtained by halving the time step ($dt/2$) on the baseline grid. The experimentally measured data from the PIV and LDV techniques are also shown in Fig. 4a for comparison. The effect of using low-speed preconditioning and Menter's two-equation (SST) model on the baseline grid are shown in Fig. 4b. The experimental data from two different techniques (PIV and LDV) are in fair agreement with each other. The overall agreement of the baseline TLNS3D results with the experimental data is quite good. In addition, it is observed from Fig. 4a that whereas the effect of refining the grid from CG to the baseline grid is significant, further refinement in the grid (FG) has a much smaller effect on these results. Similarly, halving the time step ($dt/2$) compared to the time step used for the baseline computations had insignificant effect on the resulting solutions. We note from Fig. 4b that the two-equation turbulence model (SST) results are nearly identical to the baseline (SA) results in the near field, $y < 8$ mm, but deviate noticeably from the baseline results in regions away from the slot exit, $y > 8$ mm. On the other hand, the low-speed preconditioning results are essentially identical to the
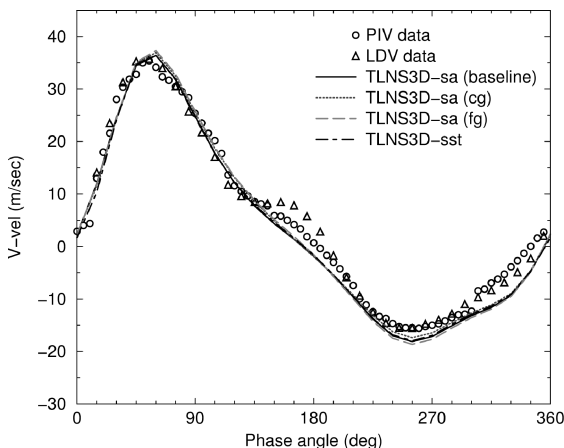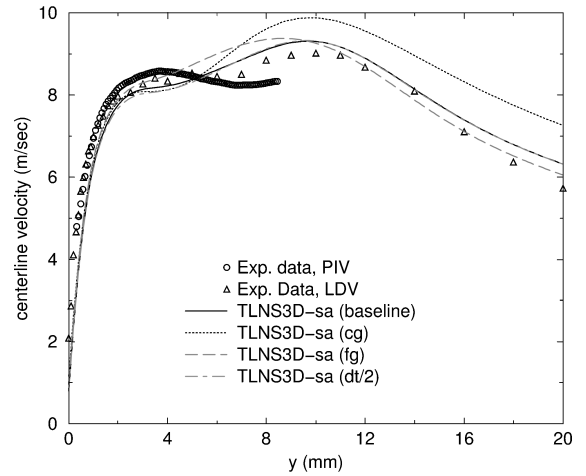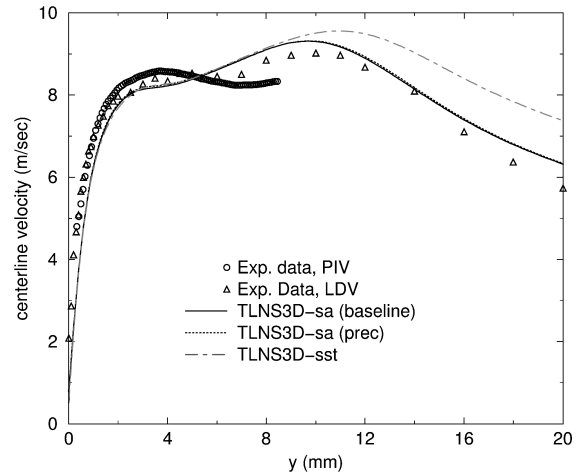

a) Effect of truncation errors

b) Preconditioning and turbulence model effects

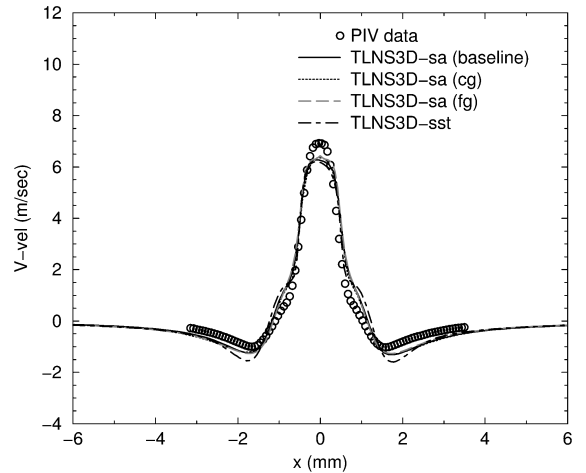**Fig. 4   Time-averaged V-VEL along centerline.**

Fig. 5   Time-averaged V-VEL at $y = 1$ mm.

baseline results. Because low-speed preconditioning[21,22,25] primarily reduces the artificial viscosity for unsteady flows, we may infer that the artificial viscosity is low in these simulations, even without preconditioning. The overall numerical accuracy of the CFD results on baseline grid with 72 time steps/period is considered quite acceptable, considering the uncertainty in physical modeling and turbulence modeling for this problem.

Figures 5 and 6, respectively, show the time-averaged V-VEL profiles at $y = 1$ and 4 mm. Except for a smaller velocity peak at

Fig. 3   Time history of V-VEL near slot exit, $x = 0$ and $y = 0.3$ mm.

$y = 1$ mm, the computational results are in very good agreement with the experimental data and with each other at these locations. Only the SST results differ visibly from the rest of the solutions. The effect of the grid refinement is also very small but grows slightly with increasing y values.

Comparing the contour plots of the time-averaged V-VEL obtained from measured PIV data and TLNS3D computations (Figs. 7a–7d) gives a global perspective of the velocity field.
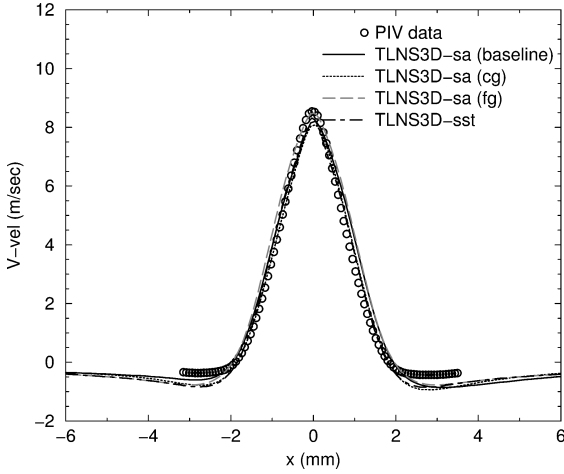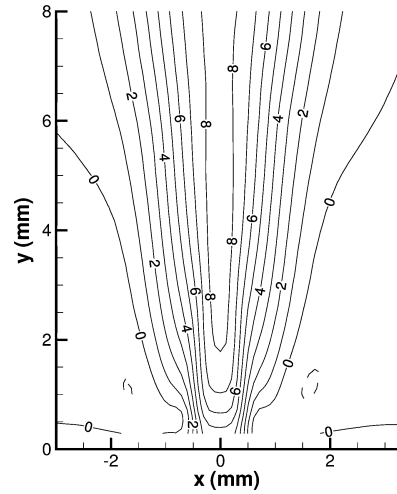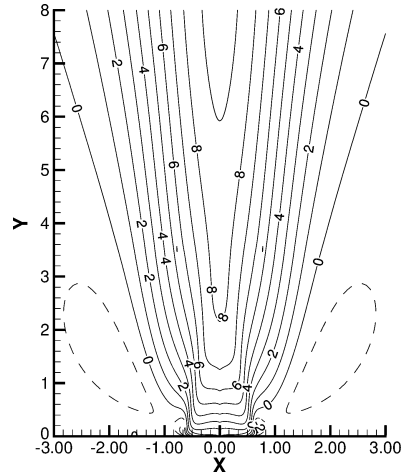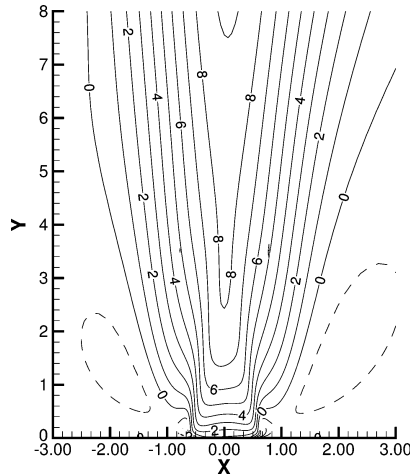

Fig. 6   Time-averaged V-VEL at $y = 4$ mm.
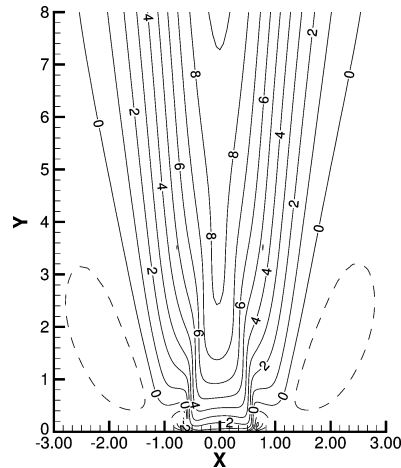
Although the computational results are available over a much larger domain, Figs. 7a–7d show a domain covering a distance of only 8 mm from the slot exit, corresponding to the region for which the high-resolution PIV data were available. We denote expulsion velocities by solid lines and suction velocities by dashed lines in Figs. 7. The computational results accurately capture all of the prominent features seen in the PIV data, including the width and spreading rate of the synthetic jet. The effect of refining the grid or using Menter's (SST) model (instead of S–A turbulence model) over this domain is quite small. The contour plots obtained with preconditioning and smaller time step (not shown here) are almost identical to the baseline results.

We now examine the phase-averaged velocities at selected locations in space and time, starting with V-VEL at $y = 2$ and 4 mm along the jet centerline. Figures 8a and 8b show the PIV and LDV data, along with TLNS3D solutions at these locations. The computational results are in fairly good agreement with the two sets of experimental data, especially in the suction phase. The agreement with the experimental data farther away from the slot exit is slightly worse during the peak expulsion cycle. In particular, the CFD results predict a delayed phase shift for the peak expulsion, reflective of a smaller convective speed for outward movement of the synthetic jet compared to the experimental data. Except for a slightly larger peak velocity for the SST model during the expulsion phase, all four sets of computational results are practically indistinguishable from one another.

Next, we compare the contour plots of the computed and measured velocities at phase angles representative of the expulsion (phase = 75 deg) and suction (phase = 255 deg) cycles.
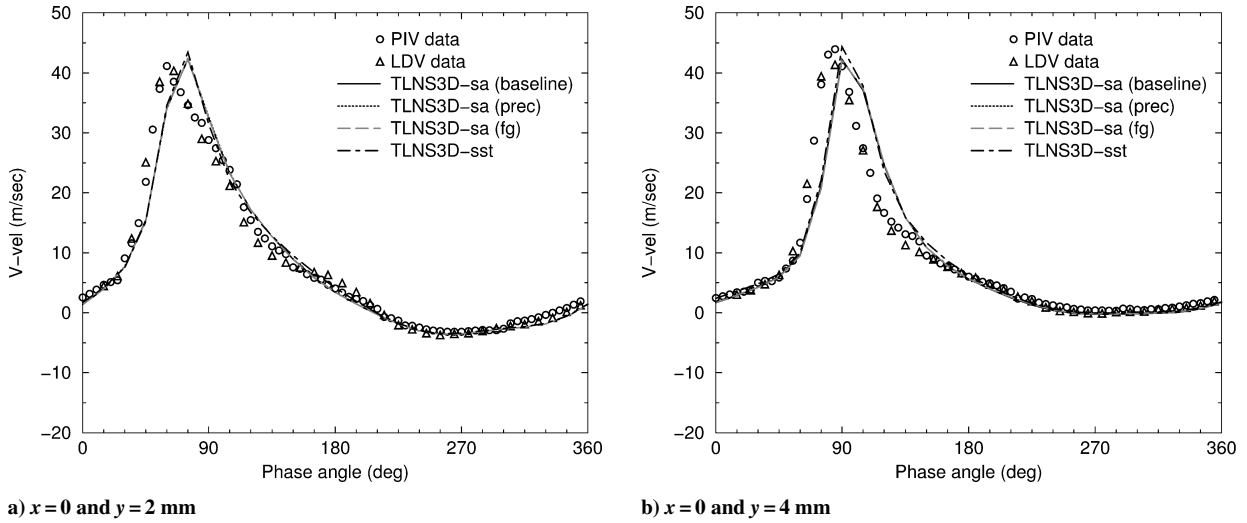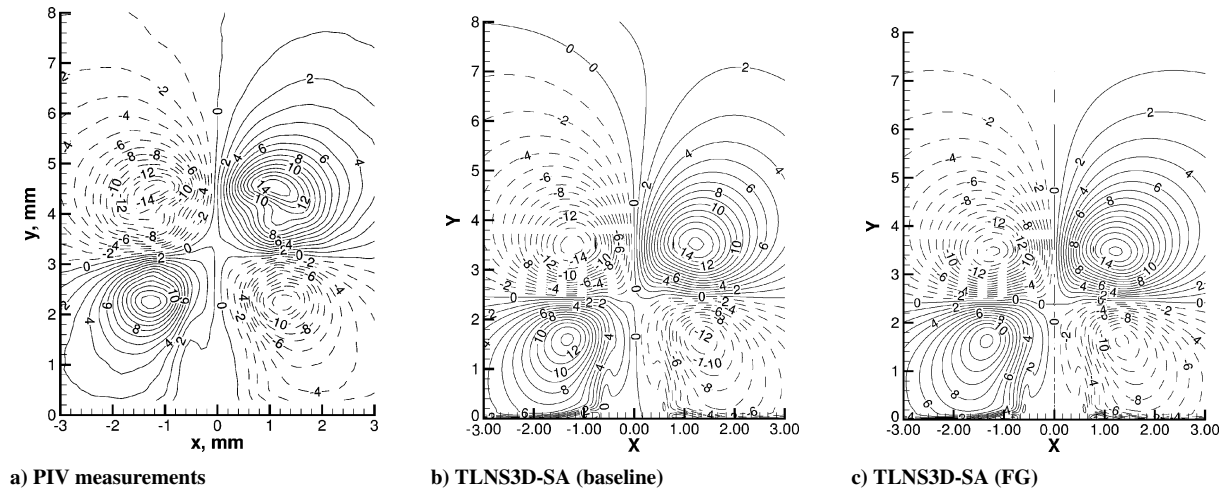

a) PIV measurements

c) TLNS3D-SA (FG)

b) TLNS3D-SA (baseline)

d) TLNS3D-SST (baseline)

Fig. 7   Time-averaged V-VEL contour comparisons.

a) $x = 0$ and $y = 2$ mm   b) $x = 0$ and $y = 4$ mm

Fig. 8   Phase-averaged V-VEL comparisons.

a) PIV measurements   b) TLNS3D-SA (baseline)   c) TLNS3D-SA (FG)

Fig. 9   Phase-averaged U-VEL contours at expulsion, phase = 75 deg.

a) PIV measurements   b) TLNS3D-SA (baseline)   c) TLNS3D-SA (FG)
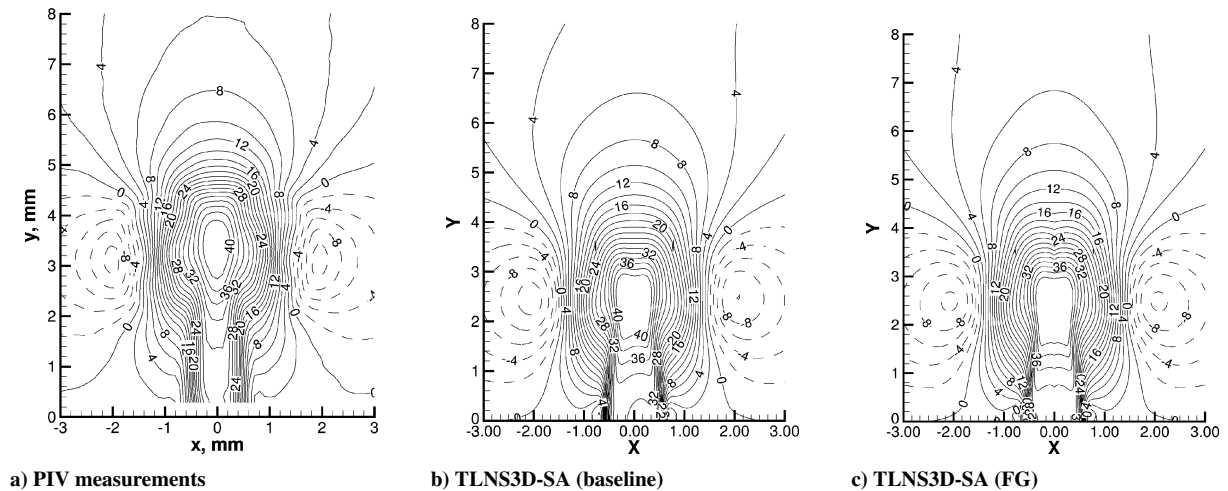
Fig. 10   Phase-averaged V-VEL contours at expulsion, phase = 75 deg.

Figures 9–12 show the contour plots for the phase-averaged horizontal velocity (U-VEL) and V-VEL obtained from the PIV data and TLNS3D computational results on baseline and FG with the S–A turbulence model. Although not shown here, the results obtained with preconditioning and SST turbulence model show very little variation from the baseline solutions. Figures 9–12 were generated using identical contour levels for both the experimental and CFD data to provide quantitative comparisons. The solid lines represent

positive values for the velocities, whereas the dashed lines represent negative values. This sign convention is helpful in identifying the flow direction and position of the vortex center. It is clear from Figs. 9–12 that the computational results capture most of the pertinent features observed experimentally and are in good agreement with the experimental data of Yao et al.[10] The largest differences during the suction phase are seen in U-VEL contours (Fig. 11) in regions away from the slot exit, where the velocities are very small
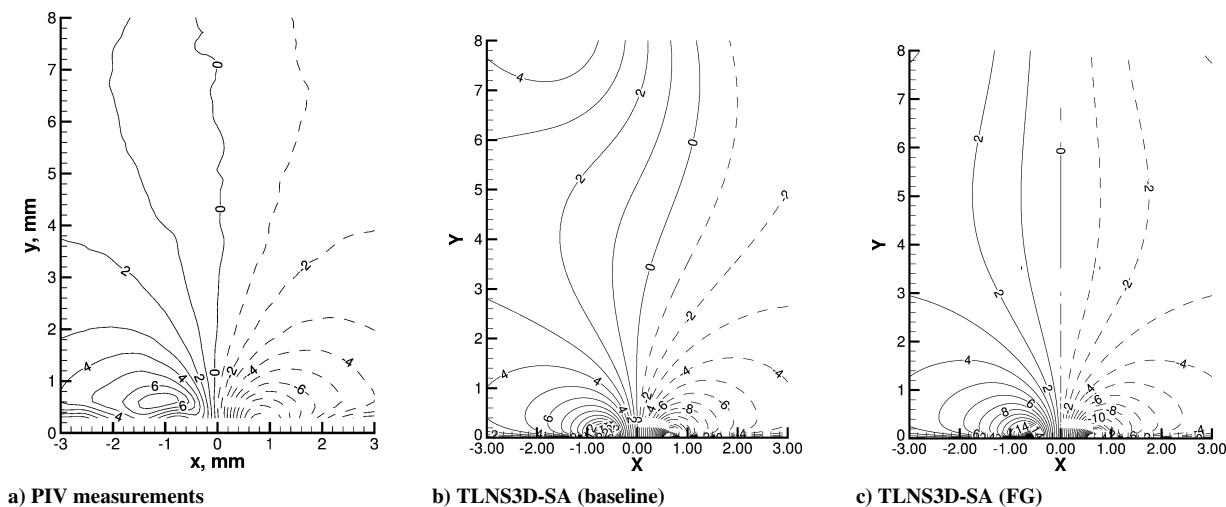
a) PIV measurements   b) TLNS3D-SA (baseline)   c) TLNS3D-SA (FG)

Fig. 11 Phase-averaged U-VEL contours at suction, phase = 255 deg.

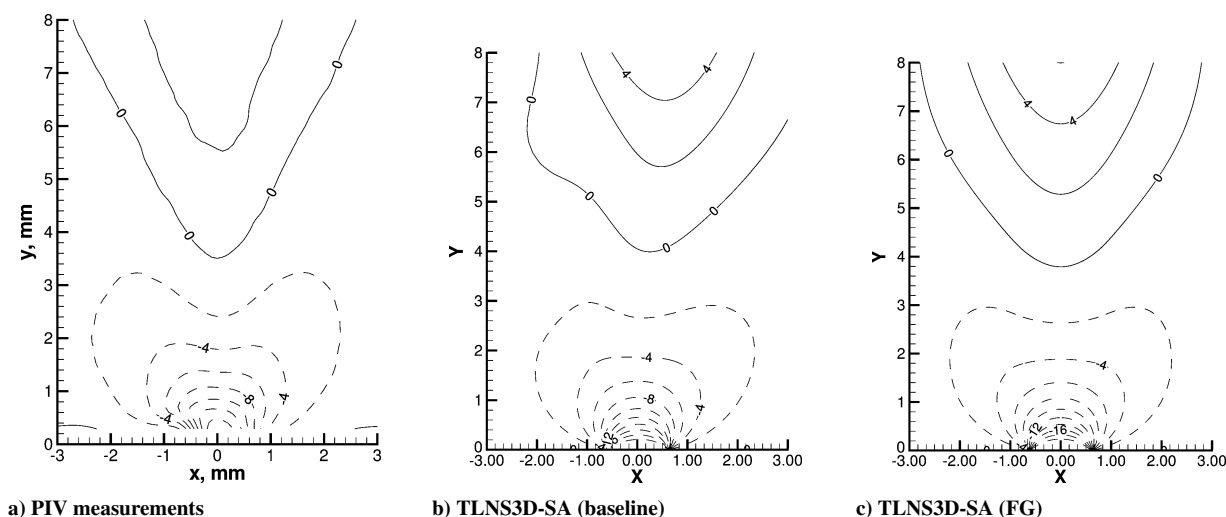a) PIV measurements   b) TLNS3D-SA (baseline)   c) TLNS3D-SA (FG)

Fig. 12 Phase-averaged V-VEL contours at suction, phase = 255 deg.

in magnitude. During the expulsion phase (Figs. 9 and 10), the computed peak velocity at the vortex center is found to be in good agreement with the PIV data, but the computed vortex center is located closer to the slot exit compared to the experimental data. Yao et al.[10] have observed increasing three-dimensional effects for this case as one moves away from the slot exit, mainly because of ring vortices formed from the slot edges. We conjecture that these ring vortices induce forces that accelerate the convection of the synthetic jet in the far field, which cannot be simulated by the two-dimensional computations.

Conclusions

Detailed comparisons have been presented for time-averaged and phase-averaged velocities between the experimental data and the computational results. Grid refinement and time-step refinement studies indicated that the numerical accuracy of the baseline solutions is quite good for engineering purposes. Low-speed preconditioning had insignificant effect on the numerical solutions. The effect of using a two-equation turbulence model of Menter (SST) was small in the near field, but was more noticeable in the far field, away from the slot exit. However, the SST model had very little effect on the strength, size, and convective speed of the primary vortex generated by the synthetic jet compared to the baseline results obtained with the S–A model. The development of the synthetic jet in the quiescent medium is driven primarily by the velocity field at the slot exit. Hence, formulating this forcing function is much

more crucial than detailed modeling of the cavity and parametric variations of the numerical algorithm. The computational results in the reduced domain with a forcing function reflecting the temporal profile at the jet exit are found to be in good agreement with the experimental data in the near field. However, the agreement with the experimental data deteriorates in regions farther away from the slot exit. Based on the available experimental data, it appears that the flow becomes three-dimensional after 5–6 slot widths away from the exit. Future work should focus on three-dimensional computations for this configuration to resolve such issues.

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